**AMENDMENTS TO THE CLAIMS:**

This listing of claims will replace all prior versions, and listings, of claims in the application:

**LISTING OF CLAIMS:**

1. (Original) A process for the conversion of syngas using a Fischer-Tropsch reactor, the process comprising:
   a) forming a first syngas;
   b) reacting at least a portion of the first syngas containing at least about 2 vol% $CO_2$ in a Fischer-Tropsch reactor to form a first hydrocarbonaceous product and a second syngas comprising at least about 2 vol% $CO_2$;
   c) mixing the second syngas with a hydrogen-containing stream to provide an adjusted syngas having a molar ratio of $H_2$:($CO+CO_2$) of at least about 1.0; and
   d) reacting at least a portion of the adjusted syngas in a dual functional syngas conversion reactor to form a second hydrocarbonaceous product and a third syngas comprising a reduced amount of $CO_2$ than was present in the adjusted syngas.

2. (Original) The process of claim 1, wherein at least a portion of the third syngas is used as a fuel in the process.

3. (Original) The process of claim 1, wherein the Fischer-Tropsch reactor is a reactor selected from the group consisting of a slurry bed reactor, a fixed bed reactor, a fluidized bed reactor and combinations thereof.

4. (Original) The process of claim 1, wherein the Fischer-Tropsch reactor is a slurry bed reactor comprising a Fischer-Tropsch catalyst that comprises cobalt.

5. (Currently Amended) The process of claim 1, wherein the dual functional syngas conversion reactor comprises a catalyst comprising at least one element selected

from the group consisting of copper, chromium, ~~alumina,~~ zinc, ~~iron, cobalt, nickel, ruthenium, thorium, rhodium, osmium~~ and combinations thereof.

6. (Original) The process of claim 5, wherein the catalyst comprises a zeolite.

7. (Original) The process of claim 6, wherein the zeolite has an MFI structure.

8. (Original) The process of claim 1, wherein the adjusted syngas has a molar ratio of $H_2$:($CO$+$CO_2$) between about 1.25 and about 3.0.

9. (Original) The process of claim 1, wherein the dual functional syngas conversion reactor is operated under conditions including a temperature between about 300°C and about 500°C and a pressure between about 25 atmospheres and about 100 atmospheres.

10. (Original) The process of claim 9, wherein the temperature is between about 375°C and about 425°C and the pressure is between about 35 atmospheres and about 75 atmospheres.

11. (Original) The process of claim 1, wherein $CO_2$ conversion in the dual functional syngas conversion reactor is between about 20% and about 80%.

12. (Original) The process of claim 1, wherein the hydrogen-containing stream mixed with the second syngas is obtained from a source selected from the group consisting of $C_6$-$C_{10}$ naphtha reformation, unreacted hydrogen from hydroprocessing a $C_{10+}$-containing feedstock, syngas and combinations thereof.

13. (Original) The process of claim 1, further comprising recovering hydrogen for use in the hydrogen-containing stream by using a recovery process selected from the group consisting of adsorption, absorption, cryogenic separation, membrane separation and combinations thereof.

14. (Original) The process of claim 1, wherein the hydrogen-containing stream mixes with the second syngas at least one of before, during or after entering the dual functional syngas reactor.

15. (Original) A process for the conversion of syngas using a Fischer-Tropsch reactor, the process comprising:

a) forming a first syngas;

b) reacting at least a portion of a blended syngas, comprising at least a portion of the first syngas and containing at least about 2 vol% $CO_2$, in a Fischer-Tropsch reactor to form a first hydrocarbonaceous product and a second syngas comprising at least about 2 vol% $CO_2$;

c) mixing the second syngas with a hydrogen-containing stream to provide an adjusted syngas having a molar ratio of $H_2$:(CO+ $CO_2$) of at least about 1.0;

d) reacting at least a portion of the adjusted syngas in a dual functional syngas conversion reactor to form a second hydrocarbonaceous product and a third syngas comprising a reduced amount of $CO_2$ than was present in the adjusted syngas; and

e) blending at least a portion of the third syngas with at least a portion of the first syngas to form the blended syngas.

16. (Original) The process of claim 15, wherein the blended syngas has a $CO_2$ content of about 15 vol% or less.

17. (Original) The process of claim 16, wherein the $CO_2$ content is about 10 vol% or less.

18 – 20. (Canceled)